

## Supplementary material: Electrooxidation treatment of simulated wastewater using mixed-metal oxide anodes for bacterial decontamination

Poulomi Chandra<sup>*a*</sup>, Diptiman Choudhury<sup>®</sup> <sup>*a*, *b*</sup> and Anoop Verma<sup>®</sup> \*, *b*, *c* 

<sup>*a*</sup> School of Chemistry and Biochemistry, Thapar Institute of Engineering and Technology (TIET), Patiala, Punjab-147004, India

 $^b$ TIET-VT (Virginia Tech-USA) Centre of Excellence for Emerging Materials (CEEMS), Thapar Institute of Engineering and Technology, Patiala, Punjab-147004, India

 $^c$  School of Energy and Environment, Thapar Institute of Engineering and Technology (TIET), Patiala, Punjab-147004, India

*E-mails*: pchandra\_phd19@thapar.edu (P. Chandra), diptiman@thapar.edu (D. Choudhury), anoop.kumar@thapar.edu (A. Verma)

<sup>\*</sup> Corresponding author.



**Supplementary Figure S1.** The graphs show the regression plot of predicted vs actual for (a) % Inactivation and (b) Eenergy consumption indicating that the actual experimental values are in close proximity with the predicted values.



Supplementary Figure S2. XRD graph of fresh and recycled MMO anode after 50 experimental runs.



Supplementary Figure S3. I–V curve of MMO anode at a scanning rate of 500 mV/s for 50 cycles.



**Supplementary Figure S4.** PL spectra of OH radical at 425 nm under optimized condition of (current density =  $6.34 \text{ mA/cm}^2$ , NaCl dose = 1.77 g, time = 10 min). (a) The graph shows the PL spectra of OH radical at an acidic pH of 3.8 when no NaCl dose was applied. (b) The graph shows the PL spectra of OH radical with NaCl dose of 1.77 g.



**Supplementary Figure S5.** (a) The graph depicts the synergistic effect of RCS and •OH of simulated wastewater containing bacterial consortium under optimized conditions of (current density =  $6.34 \text{ mA/cm}^2$ , NaCl dose = 1.77 g). (b) The graph dipicts the chloride concentration of the sample solution having bacterial consortium.

Factors	Variables	Range of actual and coded variables		
		-1	0	+1
$X_1$	NaCl dose (g/L)	0.5	1.5	2.5
$X_2$	Current density (mA/cm <sup>2</sup> )	2.38	7.14	11.90
$X_3$	Treatment time (min)	2	9	16

**Supplementary Table S1.** Range of actual and coded variables for electrooxidation treatment of simulated wastewater

Supplementary Table S2. Constraints of process variables for optimization

Variables	Goal	Lower limit	Upper limit	
j	Is in range	2.38	11.904	
n	Is in range	0.5	2.5	
t	Is in range	2	16	
% Inactivation	Maximize	1.7	99.97	
Energy consumption	Minimize	0.033	1.995	

Supplementary Table S3. Individual and multiresponse optimization for desirability calculations

Response	Current density	NaCl dose	Time	Desirability
	$(mA/cm^2)$	(g/L)	(min)	
Individual response optimization				
% Inactivation, $(Q_1) = 100.00\%$	10.35	1.05	8.01	1.000
Energy consumption, $(Q_2) = 0.022 \text{ kWh/m}^3$	2.40	0.82	2.01	1.000
Simultaneous optimization of responses				
% Inactivation, $(Q_1) = 99.96\%$	6.34	1.77	10	0.884
Energy consumption, $(Q_2) = 0.58 \text{ kWh/m}^3$				

**Supplementary Table S4.** Comparison between predicted and actual experimental values at optimized conditions

Responses	Predicted	Actual experimental values
% Inactivation	99.96%	99.2%
Energy consumption (kWh/m <sup>3</sup> )	0.58	0.42

Supplementary Table S5. Evaluation of tentative operating cost of EO process

Electrical energy consumed for treating bacteria with MMO =  $0.413 \text{ kWh/m}^3$ Price of electricity in Punjab = 0.070 kWhPrice of electricity consumption =  $0.070 \times 0.413 = 0.028 \text{ k/m}^3$ Price of one MMO anode used = 9.43 kTotal price of MMO anode = 9.43 + 0.028 = 9.458 kTotal cost of MMO for removal of bacteria =  $9.43 + 0.028 = 9.458 \text{ k/m}^3$ Total runs = 50Cost of one run =  $9.458/50 = 0.189 \text{ k/m}^3$ Total operating cost for per run of bacterial inactivation =  $0.189 \text{ k/m}^3$