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## Preparation and characterization of molybdenum hexacarbonyl encapsulated in polystyrene and its application as an efficient and reusable catalyst for epoxidation of alkenes with *tert*-BuOOH

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### 1. Introduction

Epoxidation of olefins is one of the fundamental oxidation reactions in industrial chemistry because epoxides serve as useful intermediates which can be used for synthesis of a wide variety of other compounds [1]. Transition metals such as rhenium [2], titanium [3], vanadium [4], manganese and molybdenum have been used for epoxidation of alkenes. Amongst them, Mo (VI) compounds are the most versatile catalysts for epoxidation of alkenes [5–10]. Molybdenum based catalysts in homogeneous phase as well as titanium catalysts in heterogeneous phase are applied for the production of propylene oxide with alkyl hydroperoxides as oxidant [11].

In recent years, the design and synthesis of catalytically active supported metal complexes have received considerable interest because these heterogeneous catalysts offer

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#### ABSTRACT

Molybdenum hexacarbonyl encapsulated in polystyrene, Mo(CO)<sub>6</sub>@PS, was prepared by suspension polymerization of styrene and divinylbenzene in the presence of Mo(CO)<sub>6</sub>. This catalyst was found as an efficient catalyst for epoxidation of a wide variety of alkenes, including aromatic and aliphatic terminal ones using *tert*-butyl hydroperoxide as oxidant. This new heterogenized molybdenum carbonyl catalyst could be easily recovered by simple filtration and was reused ten consecutive times without loss of its catalytic activity. © 2011 Published by Elsevier Masson SAS on behalf of Académie des sciences.

several practical advantages over their homogeneous counterparts [12–14]. In these systems, not only advantages of homogeneous catalysts such as high catalytic activity and selectivity are retained but also some properties like easier work-up, recyclability and stability of heterogeneous systems will be obtained. Different approaches have been reported for immobilization or encapsulation of molybde-num catalysts on organic polymers [15–20], silica [21–24], modified MCM-41 [25–30], and zeolites [31].

In the encapsulation, there is a direct linkage between the catalyst and the support, and it is the only method which attempts to mimic the homogeneously catalyzed reactions. Other methods, by necessity, lead to changes in the catalyst. For example, covalent tethering requires the modification of ligand (which may influence the electronic character of the ligand and/or the conformation of the ligand), and in physisorption and ion-exchange methods the catalyst should be in close proximity to the support which may also affect the electronic properties and ligand conformation.

In styrene-based copolymers, depending on the nature of the cross-linking agent, inner spaces or cavities with definite sizes are produced during the polymerization

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Scheme 1.

process [32,33]. For divinylbenzene (DVB) cross-linked polystyrene (PS), these cavities have a hydrophobic environment, and for hexanedioldimethacrylate (HDDMA) cross-linked PS, they have a hydrophilic environment. Molecules can be trapped in these pockets without recourse to chemical bonding. This method can be used for the encapsulation of guest molecules in a polymer if the size and geometry of the functionalized guest molecules are acceptable to the geometry of the cavities.

In this work, we report the encapsulation of molybdenum hexacarbonyl in the polystyrene cavities. This new heterogeneous catalyst, [Mo(CO)<sub>6</sub>]@PS derived catalyst, was characterized by FT-IR, UV–Vis and SEM. The activity and reusability of catalyst was investigated in the epoxidation of alkenes with *tert*-BuOOH (Scheme 1).

#### 2. Experimental

All materials were commercial reagent grade and obtained from Merck and Fluka. Elemental analysis was performed on a Perkin-Elmer 2400 instrument. Atomic absorption analysis was carried out on a Shimadzu 120 spectrophotometer. FT-IR spectra were obtained as potassium bromide pellets in the range 400–4000 cm<sup>-1</sup> with a Nicolet-Impact 400D instrument. Gas chromatography experiments (GC) were performed with a Shimadzu GC-16A instrument using a 2 m column peaked with silicon DC-200 or Carbowax 20m. In GC experiments, *n*-decane was used as internal standard. <sup>1</sup>H NMR spectra were recorded on a Bruker-Avance AQS 300 MHz.

# 2.1. Preparation of molybdenum hexacarbonyl encapsulated in polystyrene, [Mo(CO)<sub>6</sub>]@PS derived catalyst

The monomer, i.e., styrene (S) was treated with aqueous NaOH for removing the inhibitor and stored in a refrigerator until use. Divinylbenzene (DVB) was used as the cross-linker and purified by the same method. The 2,2'azobisisobutyronitrile (AIBN) was used as initiator. Deionized water was purged with inert gas for 1 h prior the use. In a resin kettle (250 mL) equipped with a mechanical stirrer, condenser, dropping funnel, and nitrogen inlet, poly(vinyl alcohol) (7 g, 87-89% hvdrolvzed. MW = 85 000-146 000) was dissolved in water (100 mL) by vigorous stirring at 90–95 °C. The mixture was cooled to room temperature and divinylbenzene (4.8 g, 36 mmol), styrene (0.2 g, 2 mmol), and AIBN (0.1 g, 0.6 mmol) were added to the mixture. The mixture was stirred at 65 °C (650 rpm) under a gentle stream of nitrogen. A solution of  $Mo(CO)_6$  (1 g, 3.8 mmol) in 1,2-dichloroethane (5 mL, 60 °C) was added to the reaction mixture during polymerization. The polymerization was continued with vigorous stirring under a gentle stream of nitrogen for 24 h. At the end of polymerization reaction, the mixture was cooled to room temperature and  $[Mo(CO)_6]$ @PS was washed by repeated sedimentation from water at 10 °C in a centrifuge (13 000 rpm) for 30 min. Finally, the beads were dried in a vacuum oven at 80 °C overnight [34].

### 2.2. General procedure for epoxidation of alkenes

To a 25 mL round bottom flask equipped with a magnetic stirring bar, alkene (0.25 mmol), TBHP (0.5 mmol), [Mo(CO)<sub>6</sub>]@PS derived catalyst (0.02 mmol) and 1,2-dichloroethane (4 mL) were mixed and refluxed. The reaction progress was monitored by GC. At the end of the reaction,  $Et_2O$  (20 mL) was added and filtered. The resin was thoroughly washed with  $Et_2O$  and combined washings and filtrates were purified on a silica-gel plate or a silica-gel column. IR and <sup>1</sup>HNMR spectral data confirmed the identities of the products. Blank experiment in the presence of an oxidant and using the same experimental conditions in the absence of a catalyst was also performed.

#### 2.3. Reusability of the catalyst

The reusability of  $[Mo(CO)_6]$ @PS derived catalyst was studied in the repeated epoxidation reaction of *cis*cyclooctene. The reactions were carried out as described above. At the end of each reaction, the mixture was filtered, washed with Et<sub>2</sub>O, CHCl<sub>3</sub>, THF and (CH<sub>3</sub>)<sub>2</sub>CO, dried in an oven at 80 °C and reused.



Scheme 2. Preparation of [Mo(CO)<sub>6</sub>@PS] derived catalyst.

### 3. Results and discussion

#### 3.1. Preparation and characterization of the catalyst

The  $[Mo(CO)_6]$ @PS derived catalyst was prepared via the known procedure for the suspension polymerization (Scheme 2). This may be the most well-known method of polymerization, and involves the continuous addition of monomer units to a growing free-radical chain. Initiation is a two-stage process in which, first a free radical is formed, and then this radical is added to a monomer unit. The second stage is essentially similar for all related processes; however, the first step can be achieved in a variety of ways; and the type of initiator depends on the nature of the polymerization experiment. In this method, 2,2'-azobisisobutyronitrile (AIBN) is the initiator of this freeradical process presumably because of the convenient timescale of its decomposition at 60 °C. A solid framework is formed during the polymerization using a mixture of monomers in the presence of a molecular template and a small volume of a porogenic solvent. A large excess of cross-linker ensures that the solid framework that is formed around each molecule of template is relatively rigid, such that the presence of the template creates a "cavity" in the polymer structure.

The prepared catalyst was characterized by FT-IR, SEM, diffuse reflectance UV-vis and elemental analysis.

The FT-IR spectra of cross-linked PS and  $[Mo(CO)_6]$ @PS derived catalyst are shown in Fig. 1A and 1B, respectively. The peaks at 1981 and 502 cm<sup>-1</sup> in the FT-IR spectrum of



Fig. 1. The FT-IR spectra of: (A) Crosslinked PS; and (B) [Mo(CO)<sub>6</sub>]@PS derived catalyst.



Fig. 2. The SEM images of: (A) Crosslinked PS and (B)  $[{\rm Mo}({\rm CO})_6]@{\rm PS}$  derived catalyst.

 $[Mo(CO)_6]$ @PS derived catalyst (Fig. 1B) are attributed to C = O and Mo – CO stretching bands, respectively. These bands do not observe in the FT-IR spectrum of cross-linked PS (Fig. 1A).

Fig. 2 shows the SEM images of cross-linked polystyrene and  $[Mo(CO)_6]$ @PS derived catalyst. The images clearly indicate that the prepared resins have different morphologies.

UV-Vis spectroscopy was employed in the diffuse reflectance mode for the encapsulated catalyst and cross-linked polystyrene. The latter exhibits a broad band between 200–400 nm, whereas the former shows bands at 230 and 286 nm regions which can be attributed to MLCT bands (Fig. 3). These observations clearly indicates that the  $Mo(CO)_6$  moiety has been encapsulated in the polymer network.

The metal loading of  $[Mo(CO)_6]@PS$  derived catalyst, determined by atomic absorption spectroscopy (AAS), was obtained 0.52 mmol/g.

# 3.2. The effect of solvent on the epoxidation of cyclooctene with tert-BuOOH catalyzed by [Mo(CO)<sub>6</sub>]@PS derived catalyst

First, the effect of different solvents on the catalytic activity of the resulting catalyst was investigated in the epoxidation of *cis*-cyclooctene with *tert*-butylhydroper-oxide. Amongst 1,2-dichloroethane, chloroform, carbon tetrachloride, acetonitrile, acetone and tetrahydrofurane, 1,2-dichloroethane and carbon tetrachloride were the suitable solvents because the highest epoxide yield was observed (Table 1). It seems that non-coordinate solvents



**Fig. 3.** The diffuse reflectance UV-Vis spectra of: (A) Crosslinked PS and (B) [Mo(CO)<sub>6</sub>]@PS derived catalyst.

Table 1

The effect of different solvents on the epoxidation of *cis*-cyclooctene with *tert*-BuOOH catalyzed by  $[Mo(CO)_6]$ @PS derived catalyst under reflux conditions<sup>a</sup>.

Row	Solvent	Epoxide (%) <sup>b</sup>	Time (h)
1	CH <sub>3</sub> CN	30	2.5
2	(CH <sub>3</sub> ) <sub>2</sub> CO	5	2.5
3	THF	6	2.5
4	CHCl <sub>3</sub>	27	2.5
5	CCI <sub>4</sub>	96	2.5
6	1,2-Dichloroethane	96	1.5

<sup>a</sup> Reaction conditions: *cis*-cyclooctene (0.25 mmol), *tert*-BuOOH (0.5 mmol), catalyst (0.020 g, 0.01 mmol Mo), solvent (4 mL).

<sup>b</sup> GC yield based on the starting cyclooctene.

#### Table 2

The effect of different oxidants on the epoxidation of *cis*-cyclooctene by  $[Mo(CO)_6@PS]$  derived catalyst under reflux conditions<sup>a</sup>.

Row	Oxidant	Solvent <sup>b</sup>	Epoxide(%) <sup>c</sup>	Time(h)
1	TBHP	CCl <sub>4</sub>	96	2.5
2		1,2-DCE	96	1.5
3	NaIO <sub>4</sub>	$CCl_4/H_2O^d$	No Reaction	2.5
4		CH <sub>3</sub> CN/H <sub>2</sub> O	No Reaction	2.5
5	$H_2O_2$	CCl <sub>4</sub>	4	2.5
6		CH <sub>3</sub> CN	5	2.5

<sup>a</sup> Reaction conditions: cis-cyclooctene (0.25 mmol), *tert*-BuOOH (0.5 mmol), catalyst (0.020 g, 0.01 mmol Mo).

<sup>b</sup> A 3:1 mixture of organic solvent: water was used.

<sup>c</sup> GC yield based on the starting cyclooctene.

<sup>d</sup> Tetrabutylammonium bromide (0.01 g) was used.

such as chlorinated ones are the best solvents for oxidation reactions by molybdenum based catalysts.

# 3.3. The effect of different oxidants on the epoxidation of cyclooctene catalyzed by $[Mo(CO)_6]@PS$ derived catalyst

We also investigated the ability of different oxygen donors such as *tert*-BuOOH, NaIO<sub>4</sub> and  $H_2O_2$  in the oxidation of *cis*-cyclooctene, and TBHP was chosen as oxygen donor (Table 2).

# 3.4. Catalytic alkene epoxidation with tert-BuOOH in the presence of $[Mo(CO)_6]$ @PS derived catalyst

Since homogeneous molybdenum complexes are not recoverable and reusable, therefore, we decided to design a new catalytic system based on the heterogenization of

#### Table 3

Epoxidation of alkenes with *tert*-BuOOH catalyzed by  $[Mo(CO)_6@PS]$  derived catalyst in 1,2-DCE under reflux conditions<sup>a</sup>.

Entry Alkene	Conversion (%) <sup>b</sup>	Epoxide selectivity (%)	Time (h)
1	96	100	1.5
2	42	69	3
3	28	43	3.5
4	58	26	5.5
5	84	100	7
6	78	100	10

<sup>a</sup> Reaction conditions: alkene (0.25 mmol), *tert*-BuOOH (0.5 mmol), catalyst (0.020 g, 0.01 mmol Mo) and 1,2-dichloroethane (4 ml).
<sup>b</sup> GLC yield based on starting alkene.

#### Table 4

Epoxidation of alkenes with tert-BuOOH catalyzed by [Mo(CO)<sub>6</sub>@PS] derived catalyst in CCl<sub>4</sub> under reflux conditions<sup>a</sup>.

Entry	Alkene	Conversion (%) <sup>b</sup>	Epoxide Selectivity (%)	Time (h)
1		96	100	2.5
2		49	90	7
3		95	81	3
4		80	69	5
5	~~~//	93	100	3.5
6	~~~~/	87	100	10

<sup>a</sup> Reaction conditions: alkene (0.25 mmol), tert-BuOOH (0.5 mmol), catalyst (0.020 g, 0.01 mmol Mo) and CCl<sub>4</sub> (4 ml).

<sup>b</sup> GLC yield based on starting alkene.

Table 5

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Under the optimized conditions, the epoxidation of different alkenes with TBHP was carried out in the presence of [Mo(CO)<sub>6</sub>]@PS derived catalyst in 1,2dichloroethane (Table 3) and carbon tetrachloride (Table 4). This catalyst efficiently catalyzed the epoxidation of both cyclic and linear alkenes with TBHP. 1-Octene and 1- dodecene as linear alkenes were efficiently converted to their corresponding epoxides by [Mo(CO)<sub>6</sub>]@PS derived catalyst in both solvents. Cyclooctene was also epoxidized in high yield with 100% selectivity both in CCl<sub>4</sub> and 1,2-DCE. But very different results were obtained for oxidation of cyclohexene, styrene and  $\alpha$ -methylstyrene. The epoxide selectivities for cyclohexene were 90 and 69% in CCl<sub>4</sub> and 1,2-DCE, respectively. In the case of styrene and  $\alpha$ methylstyrene, the conversions in CCl<sub>4</sub> were 95 and 80% with 81 and 69% selectivity, respectively, while in 1,2-DCE, both conversions and selectivities were lower.

#### 3.5. Catalyst reusability

The reusability of the catalysts was monitored using multiple sequential epoxidation of *cis*-cyclooctene with TBHP (Table 5). To assess long-term stability and reusability of  $[Mo(CO)_6]$ @PS derived catalyst, epoxidation of *cis*-cyclooctene was chosen as model reaction, and recycling experiments were carried out with a single sample of the catalyst. After each experiment, the catalyst was removed by simple filtration, washed with Et<sub>2</sub>O and dried in an oven at 50 °C and reused. After reusing the catalyst for ten consecutive times, the conversion was 90%

Run	Epoxide (%) <sup>b</sup>	Time (h)	Mo leached (%) <sup>c</sup>
1	96	1.5	2
2	92	1.5	0
3	91	1.5	0
4	91	1.5	0
5	91	1.5	0
6	91	1.5	0
7	91	1.5	0
8	91	1.5	0
9	91	1.5	0

Reusability of [Mo(CO)<sub>6</sub>]@PS derived catalyst in the epoxidation of

cyclooctene in the presence of TBHP under reflux conditions<sup>a</sup>

<sup>a</sup> Reaction conditions: alkene (0.5 mmol), *tert*-BuOOH (1 mmol), catalyst (0.010 g of supported catalyst, 0.016 mmol Mo) and 1,2-dichloroethane (3 ml).

1.5

0

<sup>b</sup> GLC yield based on the starting alkene.

<sup>c</sup> Determined by ICP.

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(Table 5). No molybdenum was detected in the filtrates by ICP measurement after first run. The nature of the recovered catalyst was studied by FT-IR spectra, in which the CO bands have disappeared in its FT-IR spectra (Fig. 4). On the other hand, the DR UV-vis of the recovered catalyst (Fig. 5) is different from initial catalyst which is in accordance with FT-IR spectrum. The mechanism of these reactions has been previously reported [35,36]. Upon reaction of [Mo(CO)<sub>6</sub>] with TBHP, the Mo = O species are produced and act as catalytic active species. The appearance of a band at 1071 cm<sup>-1</sup> in the FT-IR of recovered catalyst can be attributed to the presence of Mo = O species. Therefore, [Mo(CO)<sub>6</sub>] may be considred as a catalyst precursor.



Fig. 4. The FT-IR spectrum of recovered catalyst.



Fig. 5. The diffuse reflectance UV-Vis spectrum of recovered catalyst.

### 4. Conclusion

In conclusion, molybdenum hexacarbonyl encapsulated into polystyrene,  $Mo(CO)_6@PS$  derived catalyst, which was prepared by suspension polymerization of styrene and divinylbenzene in the presence of  $Mo(CO)_6$  derived catalyst, was used as an efficient catalyst for epoxidation of a wide variety of alkenes, including aromatic and aliphatic terminal alkenes using *tert*-butylhydroperoxide. The new heterogenized molybdenum carbonyl epoxidation catalyst was recovered by simple filtration and showed no appreciable loss of activity even after ten times of recycling.

#### References

- R.A. Sheldon, J.K. Kochi, Metal-Catalysed Oxidations of Organic Compounds, Academic Press, New York, 1981.
- [2] W.A. Herrmann, R.W. Fischer, D.W. Marz, Angew. Chem. Int. Ed. Engl. 30 (1991) 1638–1641.

- [3] T. Maschmeyer, F. Rey, G. Sankar, Nature 378 (1995) 159-162.
- [4] C.H. Behrens, K.B. Sharpless, Aldrichim. Acta 16 (1983) 67-80.
- [5] G. Grivani, S. Tangestaninejad, M.H. Habibi, V. Mirkhani, Catal. Commun. 6 (2005) 375–378.
- [6] W.R. Thiel, T. Priermeier, Angew. Chem. Int. Ed. Engl. 34 (1995) 1737– 1738.
- [7] W.R. Thiel, J. Eppinger, Chem. Eur. J. 3 (1997) 696–705.
- [8] M.M. Miller, D.C. Sherrington, J. Catal. 152 (1995) 368-376.
- [9] F.E. Kuhn, A.D. Lopes, A.M. Santos, E. Herdtweck, J.J. Haider, C.C. Romao, A.M. Santos, J. Mol. Catal. A: Chem 151 (2000) 147–160.
- [10] F.E. Kuhn, A.M. Santos, I.S. Goncalves, C.C. Romao, A.D. Lopes, Appl. Organometal. Chem 15 (2000) 43–50.
- [11] U. Arnold, R.S. da Cruz, D. Mandelli, U. Schuchardt, J. Mol. Catal. A: Chem. 165 (2001) 149–158.
- [12] M.H. Valkenberg, W.F. Holderich, Catal. Rev. 44 (2002) 321-374.
- [13] D. Trong On, D. Desplantier-Giscard, C. Danumah, S. Kaliaguine, Appl. Catal. A: Gen 222 (2001) 299–357.
- [14] A. Taguchi, F. Schuth, Micropor. Mesopor. Mater. 77 (2004) 1-45.
- [15] M.M. Miller, D.C. Sherrington, S. Simpson, J. Chem. Soc. Perkin Trans. 2 (1994) 2091–2096.
- [16] R. Mbeleck, K. Ambroziak, B. Saha, D.C. Sherrington, React. Polym. 67 (2007) 1448–1457.
- [17] G. Grivani, S. Tangestaninejad, M.H. Habibi, V. Mirkhani, M. Moghadam, Appl. Catal. A: Gen 299 (2006) 131–136.
- [18] S. Tangestaninejad, M.H. Habibi, V. Mirkhani, M. Moghadam, G. Grivani, Inorg. Chem. Commun. 9 (2006) 575–578.
- [19] S. Velusamy, M. Ahamed, T. Punniyamurthy, Org. Lett. 6 (2004) 4821– 4824.
- [20] S.V. Kotov, E. Balbolov, J. Mol. Catal. A: Chem. 176 (2001) 41-48.
- [21] P.C. Bakala, E. Briot, L. Salles, J.M. Brégeault, Appl. Catal. A: Gen 300 (2006) 91–99.
- [22] J. Jarupatrakorn, M.P. Coles, T. Don Tilley, Chem. Mater. 17 (2005) 1818-1828.
- [23] G. Wang, L.S. Feng, R.L. Luck, D.G. Evans, Z.Q. Wang, X. Duan, J. Mol. Catal. A: Chem 241 (2005) 8–14.
- [24] S. Tangestaninejad, M. Moghadam, V. Mirkhani, I. Mohammadpoor-Baltork, K. Ghani, Inorg. Chem. Commun. 11 (2008) 270–274.
- [25] S.M. Bruno, J.A. Fernandes, L.S. Martins, I.S. Gonçalves, M. Pillinger, P. Ribeiro-Claro, J. Rocha, A.A. Valente, Catal. Today 114 (2006) 263–271.
- [26] A. Sakthivel, M. Abrantes, A.S.T. Chiang, F.E. Kühn, J. Organomet. Chem. 691 (2006) 1007–1011.
- [27] A. Sakthivel, J. Zhao, G. Raudaschl-Sieber, M. Hanzlik, A.S.T. Chiang, F.E. Kühn, Appl. Catal. A: Gen 281 (2005) 267–273.
- [28] M. Abrantes, S. Gago, A.A. Valente, M. Pillinger, I.S. Gonçalves, T.M. Santos, J. Rocha, C.C. Romão, Eur. J. Inorg. Chem. (2004) 4914–4920.
- [29] S. Tangestaninejad, M. Moghadam, V. Mirkhani, I. Mohammadpoor-Baltork, K. Ghani, J. Iran. Chem. Soc. 5 (2008) S71–S79.
- [30] S. Tangestaninejad, M. Moghadam, V. Mirkhani, I. Mohammadpoor-Baltork, K. Ghani, Catal. Commun 10 (2009) 853–858.
- [31] A. Sakthivel, J. Zhao, F.E. Kühn, Catal. Lett. 102 (2005) 115–119.
- [32] S. Jing-She, A.W. Mitchell, Macromolecules 38 (2005) 8300–8307.
- [33] M. Joseph, T. Mathew, S. Devipriya, S. Kuriakose, J. Appl. Polym. Sci. 93 (2004) 1816–1824.
- [34] A. Flores, D. Cunliffe, M.J. Whitcombe, E.N. Volfson, J. Appl. Polym. Sci. 77 (2000) 1841–1850.
- [35] S. Bhaduri, D. Mukesh; In: Homogeneous Catalysis, Mechanism and Industrial Application, John-Wiley & Son, Inc. Canada (2000) 183.
- [36] M. Moghadam, S. Tangestaninejad, V. Mirkhani, I. Mohammadpoor-Baltork, A. Mirjafari, N. S. Mirbagheri, J. Mol. Catal. A: Chem. 329 (2010) 44-49.